



Redox-mediated electrosynthesis of ethylene oxide from CO₂ and water

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The electrochemical production of ethylene oxide (EO) from CO₂, water and renewable electricity could result in a net consumption of CO₂. Unfortunately existing electrochemical CO₂-to-EO conversions show impractical Faradaic efficiency (FE) and require a high energy input. Here we report a class of period-6-metal-oxide-modified iridium oxide catalysts that enable us to achieve improved CO₂-to-EO conversion. Among barium, lanthanum, cerium and bismuth, we find that barium-oxide-loaded catalysts achieve an ethylene-to-EO FE of 90%. When we pair this with the oxygen reduction reaction at the cathode, we achieve an energy input of 5.3 MJ per kg of EO, comparable to that of existing (emissions-intensive) industrial processes. We have also devised a redox-mediated paired system that shows a 1.5-fold higher CO₂-to-EO FE (35%) and uses a 1.2 V lower operating voltage than literature benchmark electrochemical systems.

The manufacture of chemicals produces a significant global carbon footprint:^{1–3} for example, direct CO₂ emissions from the production of high-value chemicals (that is, ethylene, propylene and benzene/toluene/xylene derivatives) now exceed 200 Mtyr⁻¹. In the case of ethylene oxide (EO), a commodity chemical produced at the rate of 20 Mtyr⁻¹ for the manufacture of polyethylene terephthalate, the steam cracking process emits ~1–2 tCO₂ per tonne of ethylene (C₂H₄) produced, and the direct C₂H₄ oxidation process emits ~0.9 tCO₂ per tonne of EO produced⁴.

Renewable-electricity-powered electrochemical processes convert waste CO₂ emissions into valuable chemicals and fuels such as C₂H₄, ethanol and acetate⁵, enabling a reduction in net CO₂ emissions. Additional CO₂ savings can be achieved by electrifying the upgrade of chemicals to higher-value commodities such as EO^{6–10}. For instance, the synthesis of EO from CO₂, water and renewable electricity can consume of 2 tCO₂ tEO⁻¹, in contrast to the emission of ~2 tCO₂ tEO⁻¹ from the existing process.

The electrosynthesis of EO from CO₂ is currently achieved using two independent electrolyzers: in the first CO₂ is reduced to C₂H₄; in the second C₂H₄ is oxidized to EO (ethylene oxidation reaction (EtOR))⁶. While the EtOR (Fig. 1a) was achieved at a high (1 A cm⁻²) current density, the total CO₂-to-EO Faradaic efficiency (FE) was limited to 6% when operated at a high CO₂ gas flow rate of 50 sccm (calculated from the FE for CO₂-to-C₂H₄ reduction multiplied by the FE for C₂H₄-to-EO oxidation)⁶. This literature benchmark system suffers from a major missing FE component in C₂H₄-to-EO, the loss here exceeding 80%, the result of hypochlorous acid (HOCl) cleavage to unreactive ClO⁻ in the EtOR. As a result, the energy required is ~19 MJ per kg of EO, approximately five times more

energy-intensive than the existing thermochemical route at ~4 MJ per kg of EO (ref. 7).

In this article we prepare catalysts by loading a class of period-6-metal oxides on IrO₂. We find that barium-oxide-loaded catalysts suppress HOCl cleavage and improve the C₂H₄-to-EO FE. Moving the cathode reaction over to oxygen reduction enables a total CO₂-to-EO FE of 35% with a 1.2 V lower operating voltage compared with previous literature⁶.

Results

Tuning HOCl cleavage energy on period-6-metal oxides. We first studied the HOCl cleavage process on bare IrO₂ with the aid of density-functional theory (DFT) calculations: both perfect and oxygen-vacancy-bearing IrO₂ surfaces presented a spontaneous reaction for *HOCl → *H + *OCl with negative values in Gibbs free energy change (ΔG) (Fig. 1b and Supplementary Fig. 1). The negative ΔG explains the low FE of EO on bare IrO₂ catalyst reported previously⁶, which arises from HOCl-to-ClO⁻ cleavage (Fig. 1c).

We therefore looked for ways to enhance the FE of EO on IrO₂ catalysts. By loading four period-6-metal oxides (barium, lanthanum, cerium and bismuth oxides)—known to possess good stability in chlorine solution—as promoter candidates, we sought to influence the thermodynamics of HOCl cleavage and to maintain the HOCl generation capacity. We studied these four period-6-metal-oxide-loaded catalysts (Supplementary Figs. 2–4) and investigated their performance in the electrochemical production of EO from C₂H₄ (Supplementary Fig. 5).

Of these catalysts, the barium-oxide-loaded IrO₂ (BaO_x/IrO₂) showed the best results: it limited the FE toward unreactive ClO⁻ to below 10%, thus increasing the C₂H₄-to-EO FE to 90% (Fig. 1d).

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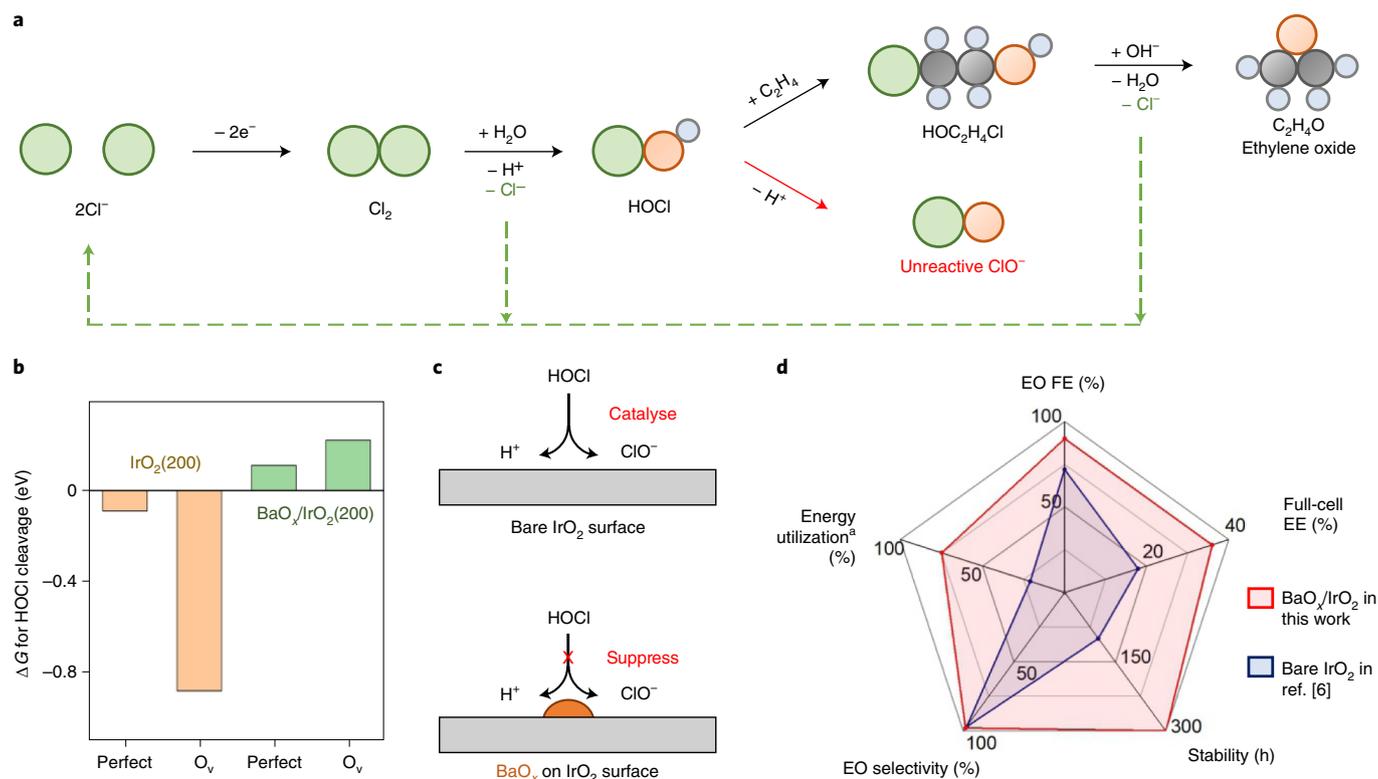


Fig. 1 | Comparison of $\text{BaO}_x/\text{IrO}_2$ and bare IrO_2 electrocatalysts. **a**, Key reaction pathway to produce EO using HOCl as the key intermediate. The HOCl-to- ClO^- cleavage will result in loss of FE toward the desired product EO. Green, chlorine; orange, oxygen; light blue, hydrogen; grey, carbon. **b**, Gibbs free energy changes (ΔG) of the reaction $^*\text{HOCl} \rightarrow ^*\text{H} + ^*\text{ClO}^-$ on bare $\text{IrO}_2(200)$ and BaO_x -cluster-loaded $\text{IrO}_2(200)$ with perfect and oxygen-vacancy (O_v) surfaces. **c**, Schematic HOCl cleavage process on bare IrO_2 and $\text{BaO}_x/\text{IrO}_2$ surfaces. Undesired HOCl cleavage can be suppressed using $\text{BaO}_x/\text{IrO}_2$ and is facilitated by bare IrO_2 . **d**, EO FE, full-cell EE, stability, EO selectivity and energy utilization compared to best prior results for EO electrosynthesis. Data are collected at the same applied current density of 100 mA cm^{-2} . ^aNormalization: for energy utilization, 100% represents the direct C_2H_4 oxidation process (the corresponding energy consumption is $\sim 4 \text{ MJ per kg}$ of EO produced).

DFT results show positive ΔG for HOCl cleavage on both perfect and oxygen-vacancy-bearing $\text{BaO}_x/\text{IrO}_2$ interfaces, suggesting that this undesired reaction becomes no longer spontaneous (Fig. 1c), thus enhancing the FE of EO (Supplementary Note 1).

We then characterized $\text{BaO}_x/\text{IrO}_2$ catalysts and determined a Ba/Ir ratio of $\sim 3 \text{ wt}\%$ (see Methods for details). The X-ray diffraction pattern suggests the presence of amorphous BaO_x species ($x = 1-2$) in the catalyst (Supplementary Fig. 6). We further explored the structure and composition of the catalyst by transmission electron microscopy (TEM) (Fig. 2a-d): the Ir, Ba and O are homogeneously dispersed throughout the nanoparticle-like catalyst, and a BaO_x nanoparticle $\sim 30 \text{ nm}$ in size is found in Fig. 2c. This suggests that some of the BaO_x nanoparticles are loaded onto IrO_2 , rather than Ba doping the IrO_2 lattice. This can be accounted for by reference to the large difference in the atomic radii (268 pm for Ba and 202 pm for Ir). We measured the lattice fringes to be 0.23 nm (Fig. 2e), and associate these with $\text{IrO}_2\{200\}$ facets¹¹. We then investigated the valence state of each element in the $\text{BaO}_x/\text{IrO}_2$ catalyst by X-ray photoelectron spectroscopy (XPS), which indicated that Ir and Ba were in the IV and II oxidation states, respectively (Fig. 2f,g)^{12,13}. In addition, the O 1s XPS peak is assigned to the OH-Ir and O-Ir bonds (Fig. 2h)¹². Based on these findings, we concluded that the catalyst is composed of BaO_x ($x = 1-2$) nanoparticles loaded onto IrO_2 .

Performance in EO electrosynthesis. We evaluated the performance of $\text{BaO}_x/\text{IrO}_2$ in a two-electrode flow-cell set-up (see Methods for details) using a titanium mesh substrate (Supplementary Fig. 7). As presented in Fig. 3a, at current densities ranging from 100 to

$1,500 \text{ mA cm}^{-2}$, the FEs of C_2H_4 -to-EO conversion on $\text{BaO}_x/\text{IrO}_2$ catalyst are $>85\%$ and reach a plateau of $90\% \pm 1\%$ at 200 mA cm^{-2} . On the IrO_2/Ti control, the FEs for EO are $\sim 65\%$ in the same current density range, consistent with the performance reported in recent work⁶. We limited the FE toward unreactive ClO^- to below 10% on $\text{BaO}_x/\text{IrO}_2$ electrocatalyst, thus reducing the aqueous waste streams by more than three-fold compared with the bare IrO_2 catalyst, which had an FE of $\sim 30\%$ for ClO^- . We also found, by conducting in situ Raman measurements (Supplementary Fig. 8), that the Ba-O-Cl structure¹⁴ is formed on $\text{BaO}_x/\text{IrO}_2$ catalysts during reaction, consistent with the models suggested by DFT calculations (Supplementary Fig. 1).

We noted that the product selectivity in the C_2H_4 -to-EO conversion is $98\% \pm 0.3\%$, with no overoxidation to CO_2 detected. We also investigated the performance of $\text{BaO}_x/\text{IrO}_2$ catalysts with different BaO_x loadings (from 1 to 4 wt%) in various anolyte concentrations (from 1 to 3 M KCl) (Supplementary Fig. 9). Of the catalysts, 3 wt% $\text{BaO}_x/\text{IrO}_2$ in 2 M KCl anolyte exhibits the highest performance. This enables an EO full-cell energy efficiency (EE) of 36% (non- iR -corrected; i , current (in amps); R , resistance (in ohms)) at 100 mA cm^{-2} (Fig. 3b), representing a 2.5-fold improvement in EE compared with literature benchmark systems operating under similar reaction rates (Supplementary Table 1)⁶.

We carried out a techno-economic assessment (Supplementary Note 2) to assess the contribution of the $\text{BaO}_x/\text{IrO}_2$ -promoted performance to total plant-gate leveled cost (PGLC, Fig. 3b)¹⁵. Using an electricity price of $\text{US}\$0.05 \text{ kWh}^{-1}$ (refs. 6,15), we found that the system equipped with the $\text{BaO}_x/\text{IrO}_2$ catalyst is projected—for a wide current density range of 100 to $1,500 \text{ mA cm}^{-2}$ —to enable a

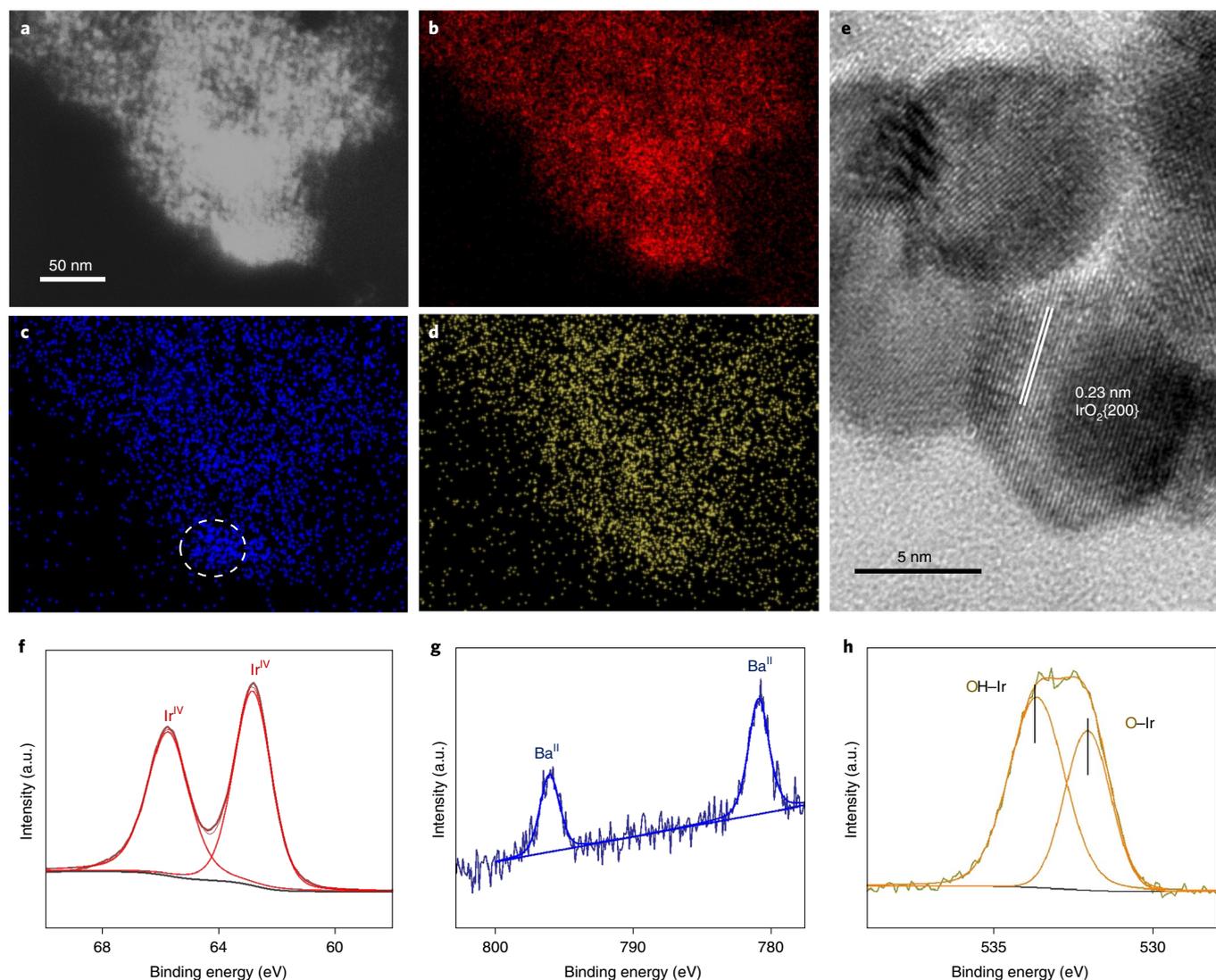


Fig. 2 | Characterization of $\text{BaO}_x/\text{IrO}_2$ electrocatalysts. **a–d**, Electron microscopy of $\text{BaO}_x/\text{IrO}_2$ catalysts: STEM image (**a**) and elemental mapping of Ir (**b**), Ba (**c**) and O (**d**). The dotted circle in **c** indicates BaO_x nanoparticles. **e**, High-resolution TEM of $\text{BaO}_x/\text{IrO}_2$ catalyst. **f–h**, Ir 4f (**f**), Ba 3d (**g**) and O 1s (**h**) XPS spectra of the as-prepared $\text{BaO}_x/\text{IrO}_2$ catalyst.

production cost that is lower than the combined market value of EO per tonne and corresponding cathodic H_2 produced (US\$1,486).

We then turned our focus to assessing the stability of the system. We performed the extended operation at a current density of 100 mA cm^{-2} , where the system delivers the highest full-cell EE with profitable PGLC. The catalyst maintains an average FE of EO of $>85\%$ and a selectivity of $\sim 98\%$ for 300 h of continuous operation with a full-cell voltage of $\sim 3.2 \text{ V}$ (non- iR -corrected) (Fig. 3c). We then analysed the structure and composition of the $\text{BaO}_x/\text{IrO}_2$ catalyst upon completion of the extended operation. The X-ray diffraction pattern, the XPS spectra and TEM images of the catalyst (Supplementary Fig. 10) suggest no obvious changes in elemental valence state, element distribution and nanoparticle-like structure. Post-reaction inductively coupled plasma atomic emission spectroscopy analysis of the catalysts indicates that the catalyst preserves its original barium loading of $\sim 3 \text{ wt}\%$ for 300 h of uninterrupted electrooxidation.

We detected ethylene chlorohydrin ($\text{HOC}_2\text{H}_4\text{Cl}$)—formed from the reaction between HOCl and C_2H_4 (Supplementary equation (3) in Supplementary note 1)¹⁶—as the only anodic product during electrolysis (Supplementary Fig. 11). We thus concluded that the

final FE of EO is only related to the amount of HOCl, because the Cl_2 will convert C_2H_4 to ethylene dichloride, which is not detected, while the other species in the anolyte (such as Cl^- and ClO^- anions) are unreactive to C_2H_4 .

We also provided the EO production performance in acidic electrolytes (pH 3 and 5; Supplementary Table 2); we found that no EO is produced. We attribute this to the absence of OH^- in acidic catholytes (Supplementary equation (4) in Supplementary note 1) and hence the suppressed conversion of $\text{HOC}_2\text{H}_4\text{Cl}$ into EO (Supplementary equation (5) in Supplementary note 1).

Full-cell optimization via anodic EtOR with the cathodic oxygen reduction reaction. Although we increased the C_2H_4 -to-EO FE to 90% by using $\text{BaO}_x/\text{IrO}_2$ catalyst, the energy input ($\sim 9 \text{ MJ}$ per kg of EO) is still 2.2-fold higher than that of the current thermochemical processes. We noted that the anodic EtOR coupled with the hydrogen evolution reaction (HER) requires a high theoretical reaction potential of 1.36 V (Fig. 4a), undesirably increasing the full-process energy requirement by producing the by-product H_2 . We posited that if we could—without sacrificing the FEs and production rates of EO—displace the HER at the cathode with a

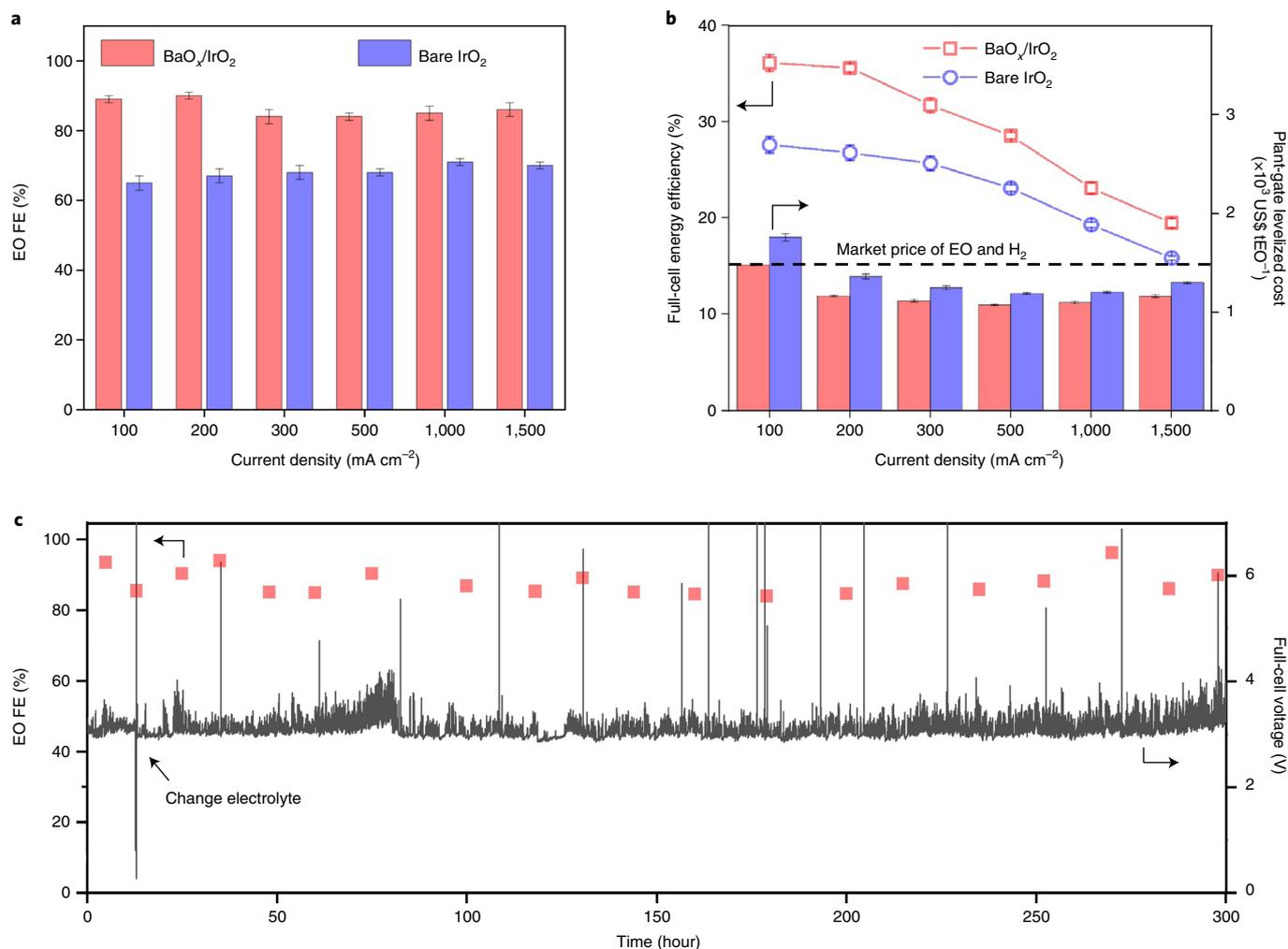


Fig. 3 | Electrochemical performance of BaO_x/IrO₂ electrocatalysts. **a, b**, The FE of EO (**a**) and the full-cell energy efficiency and PGLC (**b**) using BaO_x/IrO₂ catalysts compared with bare IrO₂ sample at different applied current densities in 2 M KCl electrolyte. The electricity cost was set at US\$0.05 kWh⁻¹. **c**, Stability test for EO during 300 h of electrolysis under a current density of 100 mA cm⁻² in 2 M KCl electrolyte. All voltages are non-*i*R-corrected. Error bars represent the s.d. from three independent measurements. Pink squares in **c** represent the EO FE. Right-angled arrows in **b** and **c** indicate the axis that is being referred to.

lower-thermodynamic-potential reaction, we would significantly reduce the energy input of the C₂H₄-to-EO conversion.

We thus replaced the HER with the oxygen reduction reaction (ORR), enabling a theoretical reaction potential of 0.13 V (Fig. 4a). At applied current densities of 100, 200 and 300 mA cm⁻², the FEs of the C₂H₄-to-EO conversion were >80% with full-cell voltages of 2.0, 2.2 and 2.4 V, respectively (Fig. 4b).

The full-cell voltage is reduced by 1.2 V compared with that of the best previous report that relied on cathodic HER (Supplementary Fig. 12)⁶. The reduction in the operating voltage in turn leads to an energy saving of 5.4 kJ per tonne of EO produced—an energy saving that corresponds to the energy required to produce H₂ in the cathodic HER case (0.045 tH₂ tEO⁻¹, equivalent to an energy of 5.4 kJ tEO⁻¹). The reduced voltage results in a PGLC reduction of US\$110 tEO⁻¹, and the loss in economic value by stopping H₂ production (0.045 tH₂ tEO⁻¹, with a value of US\$90 tEO⁻¹) is less than the saving in cost resulting from the lower reaction potential (Supplementary Fig. 13).

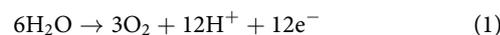
With the benefit of cathodic ORR, PGLCs in the current density range 100–300 mA cm² are projected to be profitable, with a low electrical energy input of 5.3 MJ kgEO⁻¹ (Fig. 4c), representing a 3.6-fold reduction in the energy intensity compared with the benchmark electrochemical process⁶. This energy intensity is close to that of the conventional emissions-intensive industrial process for producing

EO (~4 MJ kgEO⁻¹)⁷. It should be noted that in this electrochemical system we used the same gas feeds as the industrial direct oxidation process (air and ethylene) for producing EO with an EO selectivity of 98% while that in industry is <80%. The system was stable, maintaining an average FE of EO of >80% and a full-cell voltage of ~2 V at an applied current density of 100 mA cm⁻² for over 100 h (Fig. 4d).

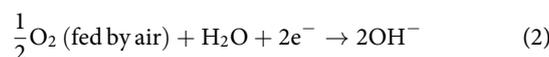
Oxygen-redox-mediated paired system for CO₂-to-EO conversion.

To test the configuration of a cathodic ORR and an anodic EtOR, we built an oxygen redox (H₂O/O₂)-mediated paired system to produce EO from CO₂ (Fig. 4e and Supplementary Fig. 14). The CO₂-to-C₂H₄ reduction in chamber 1 with C₂H₄-to-EO oxidation in chamber 2 are connected by the H₂O/O₂ mediator that cycles between the oxygen evolution reaction (OER) and the ORR (equations (1)–(3)).

On the anode side of chamber 1 for producing 1 mol of C₂H₄:



On the cathode side of chamber 2 for producing 1 mol of EO:



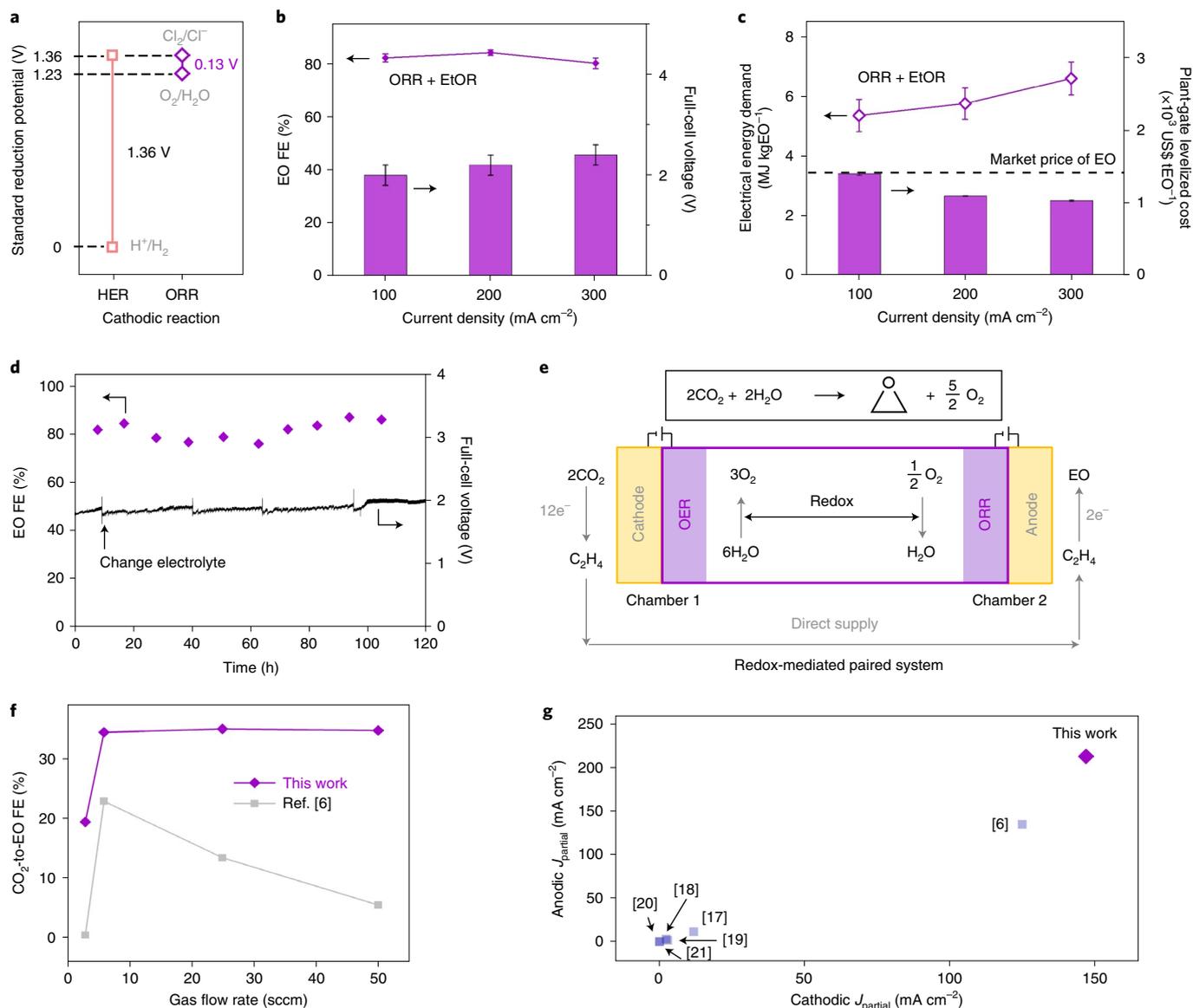
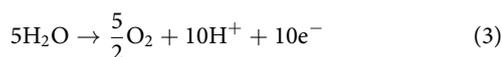


Fig. 4 | Coupling with cathodic ORR and redox-mediated paired system. **a**, Theoretical reaction potentials for producing EO for cathodic HER or ORR. **b,c**, The FE of EO and corresponding full-cell voltage (**b**) and electrical energy demand and PGELC (**c**) when coupled with the cathodic ORR at different applied current densities in 2 M KCl electrolyte. The electricity cost was set at US\$0.05 kWh^{-1} . **d**, Stability test for the production of EO during 100 h of electrolysis with cathodic ORR under a current density of 100 mA cm^{-2} in 2 M KCl electrolyte. **e**, Total reaction equation and schematic description of the electrochemical process to produce EO from CO_2 using a redox-mediated paired system with an oxygen redox mediator. **f**, Comparison of CO_2 -to-EO FEs using the $\text{BaO}_x/\text{IrO}_2$ catalysts described in this paper relative to that in the highest-performing previous reports of EO production from CO_2 and water⁶. The downstream of the CO_2 RR electrolyser was sparged into the anolyte of the C_2H_4 -to-EO oxidation flow cell (current density, 300 mA cm^{-2}) for all CO_2 flow rates studied and was used without purification. **g**, Reported cathodic and anodic partial current densities for other paired systems combining the CO_2 RR with anodic upgrading reactions^{6,17–21} (square brackets are reference numbers). Data for the redox-mediated paired system are shown in **g** for comparison (purple). All voltages are non- iR -corrected. Error bars represent the s.d. from three independent measurements. Arrows in **b** and **c**, and right-angled arrows in **d** indicate the axis that is being referred to.

In the $\text{H}_2\text{O}/\text{O}_2$ mediator (combining equations (1) and (2)):



Two approaches have been developed to produce EO from CO_2 by electrochemical means (Table 1, Supplementary Fig. 15 and Supplementary Note 3). The first involves two independent electrolyzers: one for the CO_2 reduction reaction (CO_2 RR) coupled with the OER, and another for the EtOR coupled with the HER.

The second approach involves directly coupling the CO_2 RR and the EtOR in one electrolyser. However, the first approach requires an added theoretical reaction potential of 1.23 V (Fig. 4a), and the second approach has a current matching issue that limits the anodic FE of EO to a maximum of ~17% (Supplementary note 4 and Supplementary Table 3).

The oxygen-redox-mediated paired system overcomes the above problems: we maintained a low theoretical reaction potential of 1.28 V for CO_2 -to- C_2H_4 reduction with C_2H_4 -to-EO oxidation (Table 1), and overcame the larger electron consumption in CO_2 -to- C_2H_4

Table 1 | Electrochemical systems to produce EO from CO₂

	Redox-mediated paired system	Two independent electrolyzers	One electrolyser
Cathode 1	CO ₂ -to-C ₂ H ₄	CO ₂ -to-C ₂ H ₄	CO ₂ -to-C ₂ H ₄
Anode 1	OER	OER	Cl ₂ evolution reaction (for C ₂ H ₄ -to-EO)
E ₁ ^o (V)	1.15	1.15	1.28
Cathode 2	ORR	HER	-
Anode 2	Cl ₂ evolution reaction (for C ₂ H ₄ -to-EO)	Cl ₂ evolution reaction (for C ₂ H ₄ -to-EO)	-
E ₂ ^o (V)	0.13	1.36	-
E _T ^o (V) ^a	1.28	2.51	1.28
Advantages/ challenges	<ul style="list-style-type: none"> • Low theoretical reaction potential to produce EO from CO₂ • All chambers are able to run in optimal conditions without cross-interference 	<ul style="list-style-type: none"> • All cells are able to run in optimal conditions without cross-interference • High PGLC for producing EO 	<ul style="list-style-type: none"> • Low theoretical reaction potential to produce EO from CO₂ • FE upper limit of -17% • Cross-interference (carbonate formation)

^aE_T^o = E₁^o + E₂^o; E₁^o, E₂^o and E_T^o are the theoretical reaction potentials for chamber 1, chamber 2 and total system, respectively. At pH 7, the E^o (standard reduction potential) of H⁺/H₂, O₂/H₂O, Cl₂/Cl⁻ and CO₂/C₂H₄ is -0.42, 0.81, 0.94 and -0.34 V, respectively.

(12e⁻) versus C₂H₄-to-EO (2e⁻) by converting more H₂O into O₂, rendering H₂O as the only sacrificial agent (equation (3)).

The redox-mediated electrochemical system also enables the synthesis of EO from CO₂, water and renewable electricity with a consumption of 2tCO₂tEO⁻¹, in contrast to total emissions of 2.0–2.7tCO₂tEO⁻¹ and direct emissions of 0.55tCO₂tEO⁻¹ in the existing thermochemical processes (Supplementary Fig. 16 and Supplementary Tables 4 and 5).

We produced C₂H₄ with ~45% FE from the CO₂RR at different current densities and found that the cathode and anode in chamber 1 maintain stable operation for 100 h of the CO₂RR (Supplementary Figs. 17–19 and Supplementary Table 6). We achieved a total CO₂-to-EO FE of ~35% by using the electrocatalytically generated C₂H₄ from chamber 1 at a current density of 300 mA cm⁻² with different CO₂ gas flow rates (Fig. 4f, Supplementary Fig. 20 and Supplementary Table 7). We note, for comparison, that this EO productivity is >1.5-fold higher than that reported in the literature benchmark electrocatalytic CO₂-to-EO conversion system⁶.

We also compared the performance of the redox-mediated paired system with previously described paired systems combining the CO₂RR with anodic upgrading reactions^{6,17–21}. With a total current density of 300 mA cm⁻² and high FEs, we achieved partial current densities of 147 and 213 mA cm⁻² for the cathodic C₂H₄ product and anodic EO product, respectively. These outperform by 1.5-fold the best previous reports of paired systems that combine CO₂ reduction with anodic upgrading (Fig. 4g and Supplementary Tables 8 and 9).

Discussion

In this work we sought to address the limitations of electrochemical production of EO from CO₂: we achieved an FE for CO₂-to-EO conversion that enables a 1.5-fold higher productivity compared with literature benchmark electrochemical systems. We presented a surface-modification strategy to enhance the electrochemical synthesis of EO

on period-6-metal-oxide-loaded IrO₂. Using this strategy, we found that the BaO_x/IrO₂ interface serves to block the HOCl cleavage pathway. The catalysts achieved an FE for EO of 85–91%, higher than that for the bare IrO₂ studied in our previous work⁶, and a selectivity of 98% in the current density range of 100–1,500 mA cm⁻². We obtained a stable full-cell EE of 36% at 100 mA cm⁻² for 300 h with the cathodic HER. By switching the cathodic reaction to the ORR, we achieved a 1.2 V reduction in the full-cell voltage, enabling a low energy input of 5.3 MJ per kg of EO produced electrochemically, representing a 3.6-fold reduction in energy intensity compared with the benchmark electrochemical process⁶. We further devised an O₂-redox-mediated paired system comprising CO₂-to-C₂H₄ reduction and C₂H₄-to-EO oxidation with a total FE of ~35% for complete CO₂-to-EO conversion, which means that high-rate, efficient and stable electrochemical synthesis of EO can be achieved by using CO₂, H₂O and renewable electricity as the only consumables.

Methods

Materials preparation. The electrodes for the anodic reaction were prepared by a five-step procedure. We begin by etching the titanium mesh in 3 M HCl (>98%, Sigma Aldrich) at 75 °C for 40 min. We then soak this etched mesh in a well-mixed solution of iridium(IV) oxide dehydrate (99.99%, Alfa Aesar), HCl (ACS reagent, 37%) and barium chloride dihydrate (>99.999%) (with various wt% ratios) in isopropanol (Sigma Aldrich). We then dry the resulting titanium mesh at 120 °C and sinter it at 500 °C to obtain BaO_x/IrO₂ catalyst on titanium mesh (IrO₂/Ti). Finally, we repeat the soaking, drying and sintering steps until the target BaO_x/IrO₂ loading of 2 mg cm⁻² is achieved. IrO₂/Ti electrodes were prepared by following a procedure similar to that described above, except that we instead incorporated barium chloride dihydrate salt into the catalyst ink. For X-ray diffraction measurements, a similar procedure was followed but with the BaO_x/IrO₂ catalyst supported on a hydrophilic carbon cloth (CT Carbon Cloth without MPL, Fuel Cell Store) instead of a titanium mesh, and then extracted from the surface of the carbon cloth upon completion of the synthesis. For other metal-oxide-loaded catalysts, we changed the barium precursor to 3 wt% of the corresponding metal chloride (such as lanthanum(III) chloride hydrate (99.9%), cerium(III) chloride (99.9%) and bismuth(III) chloride (99.99%)).

Electrode preparation for the redox-mediated paired system. The electrodes for the CO₂RR (chamber 1, cathode) were prepared by a two-step procedure. In the first step, copper/polytetrafluoroethylene (PTFE) electrodes were prepared by evaporating a copper target (Kurt J. Lesker) onto a hydrophobic PTFE substrate (average pore size, 450 μm) with a constant sputtering rate of 0.5 Å s⁻¹ at 10⁻⁶ torr until the desired thickness of 150 nm was achieved. In the second step, copper nanoparticle/copper/PTFE electrodes were prepared by spray-depositing a homogeneous solution of copper nanoparticles (Sigma Aldrich, 25 nm) and a polymeric binder (Aquivion D79-25BS, Sigma Aldrich) onto the copper/PTFE substrate until a catalyst loading of 1.25 mg cm⁻² was achieved.

The electrodes for the OER (chamber 1, anode) are similar to the above IrO₂/Ti electrodes. To make the electrodes for the HER and ORR (chambers 1 and 2, cathode), a well-mixed solution of commercially available platinum supported on graphitized carbon (40% Pt on Vulcan XC72, Sigma Aldrich) and polymeric binder (Aquivion D79-25BS, Sigma Aldrich) was spray-deposited on a superhydrophobic gas diffusion layer on a heated vacuum plate at 50 °C. The deposition was continued until a platinum loading of 0.4 mg cm⁻² was achieved.

Materials characterization. TEM imaging and energy-dispersive X-ray analysis elemental mapping were carried out using a field emission transmission electron microscope (Hitachi HF3300). SEM images were obtained with a Hitachi S-5200. X-ray diffraction was performed on a MiniFlex600 spectrometer with Cu Kα radiation. XPS was conducted on a Thermo Scientific K-Alpha XPS system using Al Kα X-ray radiation (1,486.6 eV) for excitation. The loading was detected via inductively coupled plasma atomic emission spectroscopy. In situ Raman spectroscopy was performed using a Renishaw inVia Raman microscope with a water immersion objective (785 nm laser) in a home-made flow cell (Supplementary Fig. 8b).

Electrochemical tests. Ethylene oxidation experiments were carried out in a flow cell equipped with an anode electrode (IrO₂/Ti), an anion-exchange membrane (Fumasep FAB-PK-130) and a cathode electrode (40% Pt on Vulcan XC72). We fabricated the cathodic and anodic flow-field plates for electrolyte delivery with thicknesses of 1.5 and 5 mm, respectively. With the thicker anodic plate, we aimed to prevent membrane leaching potentially caused by the chlorine generated in the electrochemical reaction (Supplementary equation (1) in Supplementary note 1). We fed the cathode electrode with air for the ORR, and with argon for the HER. For the anodic reaction with a reaction area of 1 cm², pure C₂H₄ from a cylinder was used as gas feed unless otherwise stated. Catholyte and anolyte (both 2 M KCl) of constant volumes of 25 ml were circulated through the electrolyser with

a constant flow rate of 10 ml min⁻¹ using a peristaltic pump equipped with silicon tubing. Upon completion of electrolysis for 1 h, we collected the samples from the anolyte container and stored these in the sealed vials for 2 d in a refrigerator before further test. Calibration was carried out using diluted solutions of the potential electrolysis products: EO and HOC₂H₄Cl. Liquid products were analysed by high-performance liquid chromatography with a Thermo Scientific Dionex UltiMate 3000 and by NMR spectrometry (Agilent DD2 600 MHz) using dimethylsulfoxide as the internal standard. The CO₂RR performance assessment of the electrodes was made using a custom-made electrochemical test station: the station consisted of a potentiostat and a booster (Metrohm Autolab, 10 A) for the control of applied potential and current, a mass flow controller (Sierra, SmartTrak 100) for the supply of CO₂, a CO₂RR membrane electrode assembly electrolyser (Dioxide Materials) for electrochemical reaction, a humidifier for CO₂ humidification, and a peristaltic pump with silicon tubing for anolyte circulation. Chamber 1 comprised anode and cathode flow-field plates made of titanium and stainless steel. The geometric flow-field areas of the anode and cathode sides were 5 cm². The anode flow channels were responsible for the uniform supply of 0.1 M KHCO₃ anolyte while the cathode flow channels were responsible for the uniform supply of humidified CO₂. Before the electrochemical assessment, the anode and cathode electrodes were placed on their respective flow-field plates, and each bolt of the electrolyser was tightened by applying an equal compression torque. For the sake of good electrical contact, the cathode electrode was attached to its flow-field plate by using a copper tape frame, which was subsequently covered via a Kapton tape frame. The electrically conductive anode electrode was mounted firmly on its flow-field plate. The anion exchange membrane was activated in 1 M KOH for at least 24 h and soaked in water for 5 min before cell assembly. Following electrolyser assembly, 0.1 M KHCO₃ anolyte was circulated through the anode flow channels at a constant flow rate of 10 ml min⁻¹ with the aid of a peristaltic pump. The humidified CO₂ was fed into the cathode flow channels at a constant flow rate of 50 sccm using a mass flow controller unless otherwise stated. The reaction was then initiated by applying a current density of interest (100, 200 and 300 mA cm⁻²). The corresponding full-cell voltage for each current density applied was recorded while concurrently collecting the gas products of the CO₂RR via a gas-tight syringe (Hamilton chromatography syringe) in a constant 1 ml volume from the cathode outlet. The gas samples collected were injected into a gas chromatography system (PerkinElmer Clarus 680) comprising three main components: a flame ionization detector, a thermal conductivity detector and packed columns. The gas chromatography spectra obtained were utilized to calculate the FEs of the gas products, including H₂, CO, CH₄ and C₂H₄. For each current density, the gas product collection was performed at least three times at suitable time intervals. The FE was calculated from the equation: FE (%) = $N \times F \times n / Q$ where N is the number of electrons transferred, F is the Farady constant, n is the number of moles of product and Q is the total charge passed in electrochemical tests.

DFT calculations. Ab initio DFT calculations were performed by applying the projector augmented-wave method²² as implemented in the Vienna Ab initio Simulation Package^{23,24}. A plane-wave cutoff of 450 eV with a $2 \times 2 \times 1$ Monkhorst-Pack k -point grid²⁵ was applied for both IrO₂ and BaO₂/IrO₂. BaO₂/IrO₂ was modelled by depositing barium oxide clusters (Ba₃O₄) on a 12-atomic-layer (4×3) supercell of IrO₂(200) surface with oxygen termination. We considered fully hydroxylated barium oxide clusters (Ba₃O₄H₄) because the saturation of oxygen atoms in metal oxide clusters is favoured in an electrochemical environment²⁶. The atomic coordinates of the optimized models are provided in Supplementary Data 1. The zero damping DFT-D3 method of Grimme et al.²⁷ was used to ensure a good description of van der Waals interactions. A standard dipole correction was also included to decouple the electrostatic interaction between the periodic images²⁸. During relaxation, atoms in the bottom-most six atomic layers of IrO₂ were fixed at their bulk positions, whereas other atoms were allowed to relax. All relaxations were considered to reach convergence until the Hellman–Feynman force on each ion was <0.01 eV Å⁻¹.

Data availability

The data supporting the findings of this study are available within the paper, the Supplementary Information and the source data files. Source data are provided with this paper.

Received: 18 July 2020; Accepted: 19 January 2022;

Published online: 24 February 2022

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Acknowledgements

This work was supported by the National Research Council Materials for Clean Fuels program (MCF-109), the Ontario Ministry of Colleges and Universities (grant ORF-RE08-034) and the Natural Sciences and Engineering Research Council (NSERC) of Canada (grant RGPIN-2017-06477). We thank P. Karimi, X. Wang, Y. C. Li, J. P. Edwards and C. P. O'Brien for discussions. Y. Li acknowledges financial support from the China Scholarship Council (201906745001). W.R.L. acknowledges financial support from an A*STAR Young Individual Research Grant (grant number A2084c0180).

Author contributions

C.L. and E.H.S. supervised the project. Y. Li, A.O. and W.R.L. conceived the idea and designed and carried out the experiments. Y. Li and W.R.L. collected STEM and TEM

images and carried out energy-dispersive X-ray spectroscopy mapping. P.O. carried out theoretical calculations. Y.X. fabricated the customized flow cell. Y. Liu and K.B. performed X-ray diffraction and XPS measurements. A.O. carried out analysis of CO₂RR products. Y. Li and W.R.L. analysed ethylene chlorohydrin and EO products. J.E.H., Y.W., C.R., H.J. and D.S. contributed to data analysis and manuscript editing. Y. Li, C.L. and E.H.S. co-wrote the paper. All authors discussed the results and assisted during manuscript preparation.

Competing interests

Y. Li, A.O., W.R.L., P.O. and E.H.S. have filed provisional patent application number 63/265.897 regarding the electrocatalysis of oxiranes. The other authors declare no competing interests.

Additional information

Supplementary information The online version contains supplementary material available at <https://doi.org/10.1038/s41929-022-00749-8>.

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Peer review information *Nature Catalysis* thanks the anonymous reviewers for their contribution to the peer review of this work.

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